



Energy Efficiency Opportunities through Combustion Optimization

CIBO Fluidized Bed Combustion & Stoker
Fired Boiler Operations and Performance
Conference

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Outline

Combustion Optimization

- What is it? &
- Why does it matter?

Technology

- What's under the hood?

Recent Case

- Review results from cases around the world

Summary

- What's the take home message?

Everybody has it, but most of us rarely talk about it

- What am I talking about here?
- It's your boiler Control System
 - Typically, 10 – 35% of loops are in manual
 - 85% have incorrect tuning parameters
 - Operators “truck drive” the boiler
- The reasons are simple
 - The process has changed but the controls haven't kept up
 - PID's fail when it comes to non-linear, large dead time processes



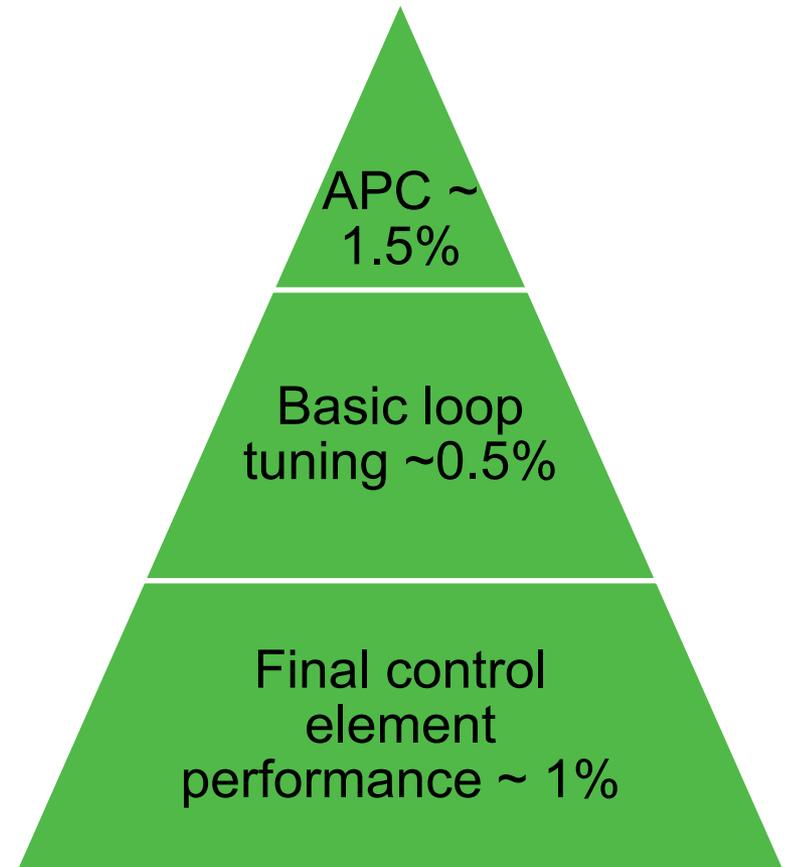
What do we mean by combustion optimization?

- **Step 1 - Automating the control loops**

- Review the major control loops
- Identify loops in manual
- Modify loops followed by tuning to ensure automatic control

- **Step 2 – Implementing Advanced Process Control (APC)**

- Identify loops with non-linear processes, variable dead times, critical constraints
- Implement fuzzy logic or model predictive control based APC's
- APC's provide setpoints to base loops or directly write to final control elements

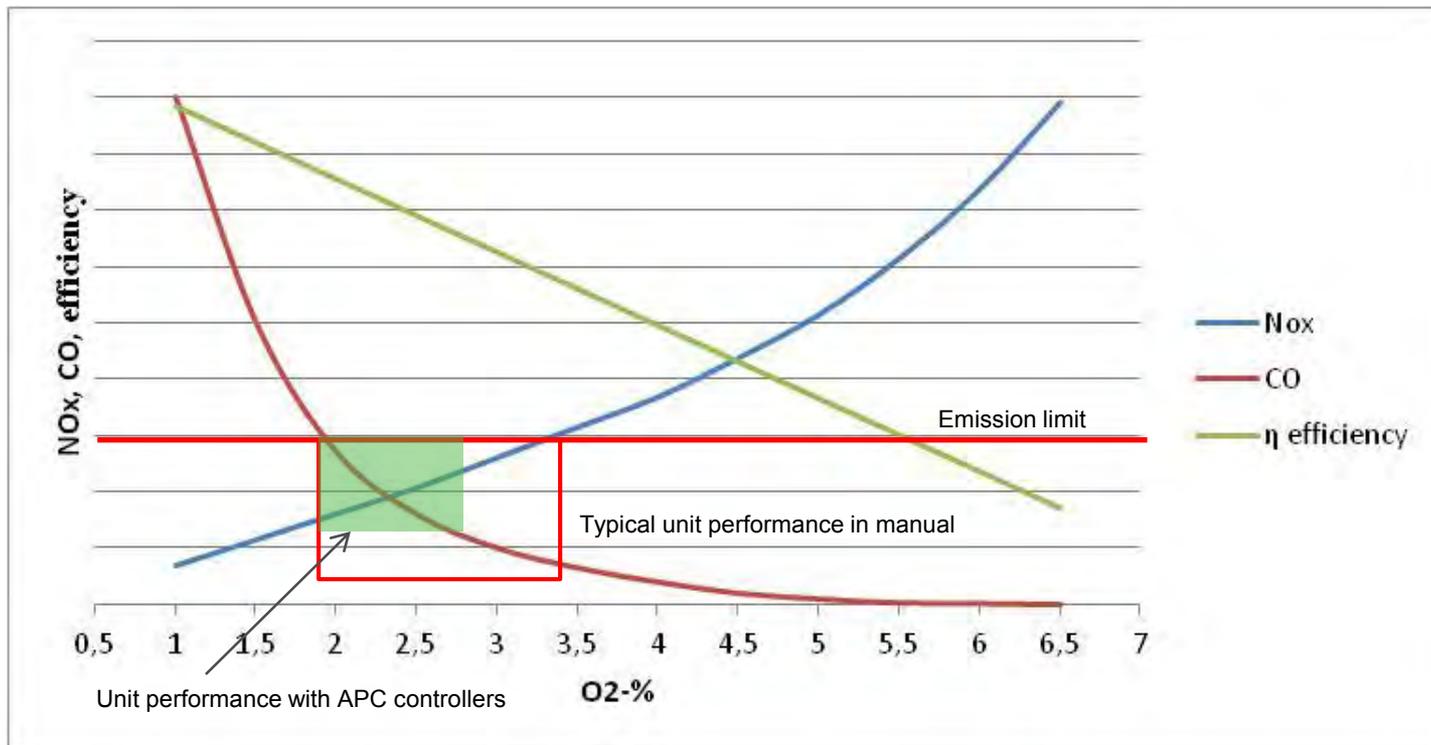


Savings as a percentage of operating costs

Brisk M.L, Process Control: Potential Benefits and Wasted Opportunities

How does it help efficiency?

Seeking optimum O₂ setpoint and air distribution for continuously changing fuel quality – minimum emissions with maximum efficiency



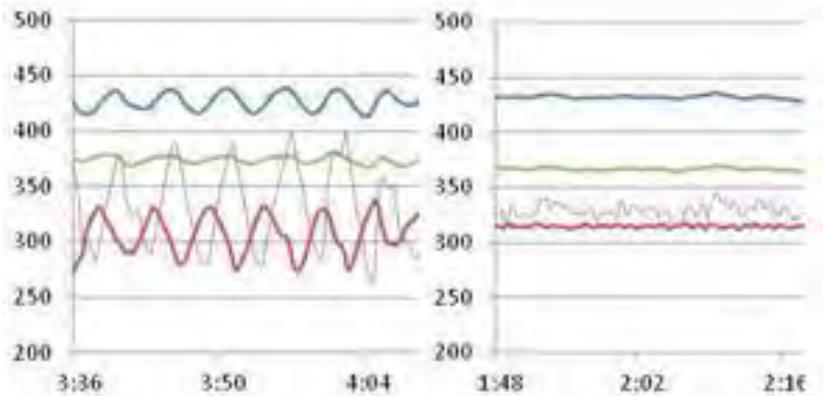
Examples of real cases from around the world

- Improvements in unit heat rate (thermal efficiency up by 1-2%)
- Reduction in emissions
(CO 67% ↓, NO_x 30% ↓)
- Reduction in reagent use such as limestone and ammonia (13% ↓)
- Increased steam output and generation
- Improved steam temperature and pressure control
- Operational uniformity across shifts



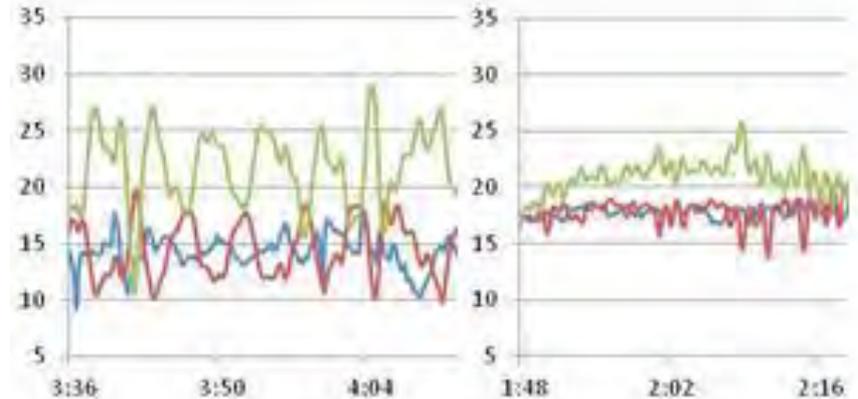
Automating base controls & enhancing where possible

Live steam temperature



— Frischdampf Temperatur [°C] — Temp. nach Einspritzung [°C]
— Temp. vor Einspritzung [°C] — Einspritzwasser Menge [t/h]

Boiler drum level

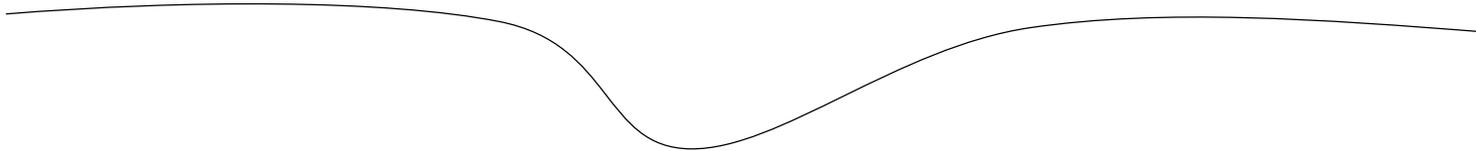


— Frischdampfmenge [t/h] — Speisewassermenge [t/h]
— Trommelniveau [mm]

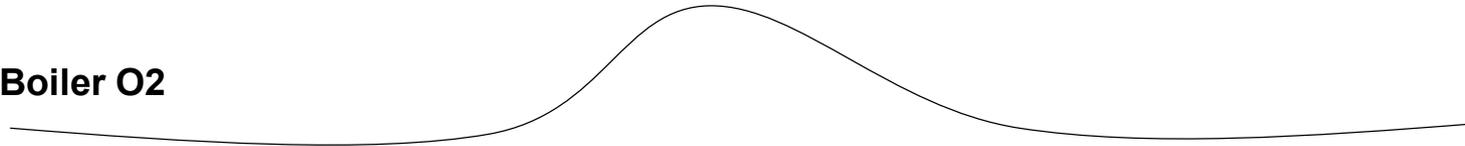
Real time fuel btu compensation

Real time fuel btu compensation

Fuel quality disturbance

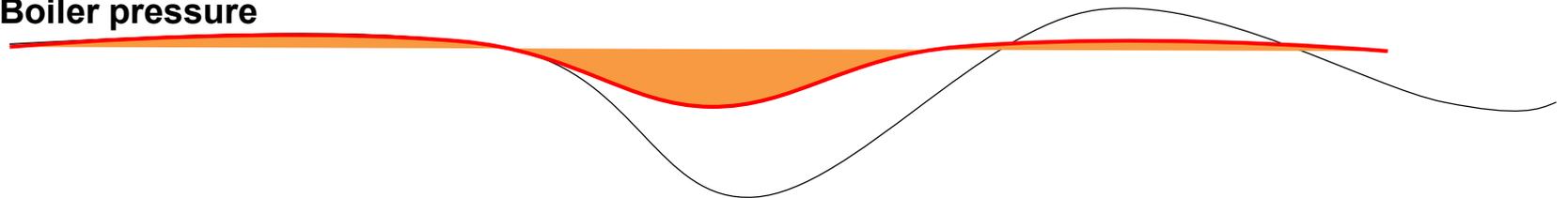


Boiler O₂

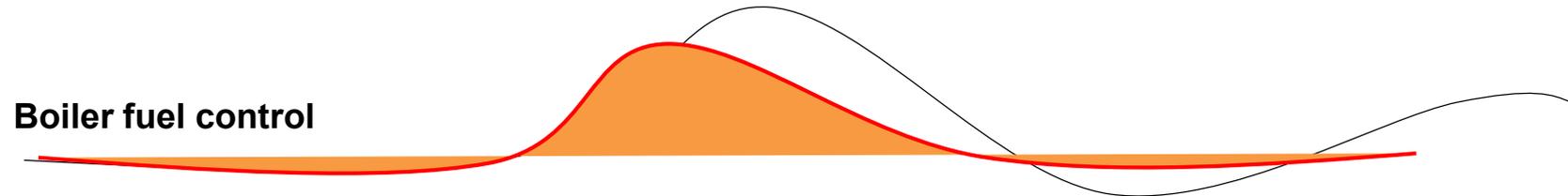


Boiler pressure

Stable pressure, no oscillation

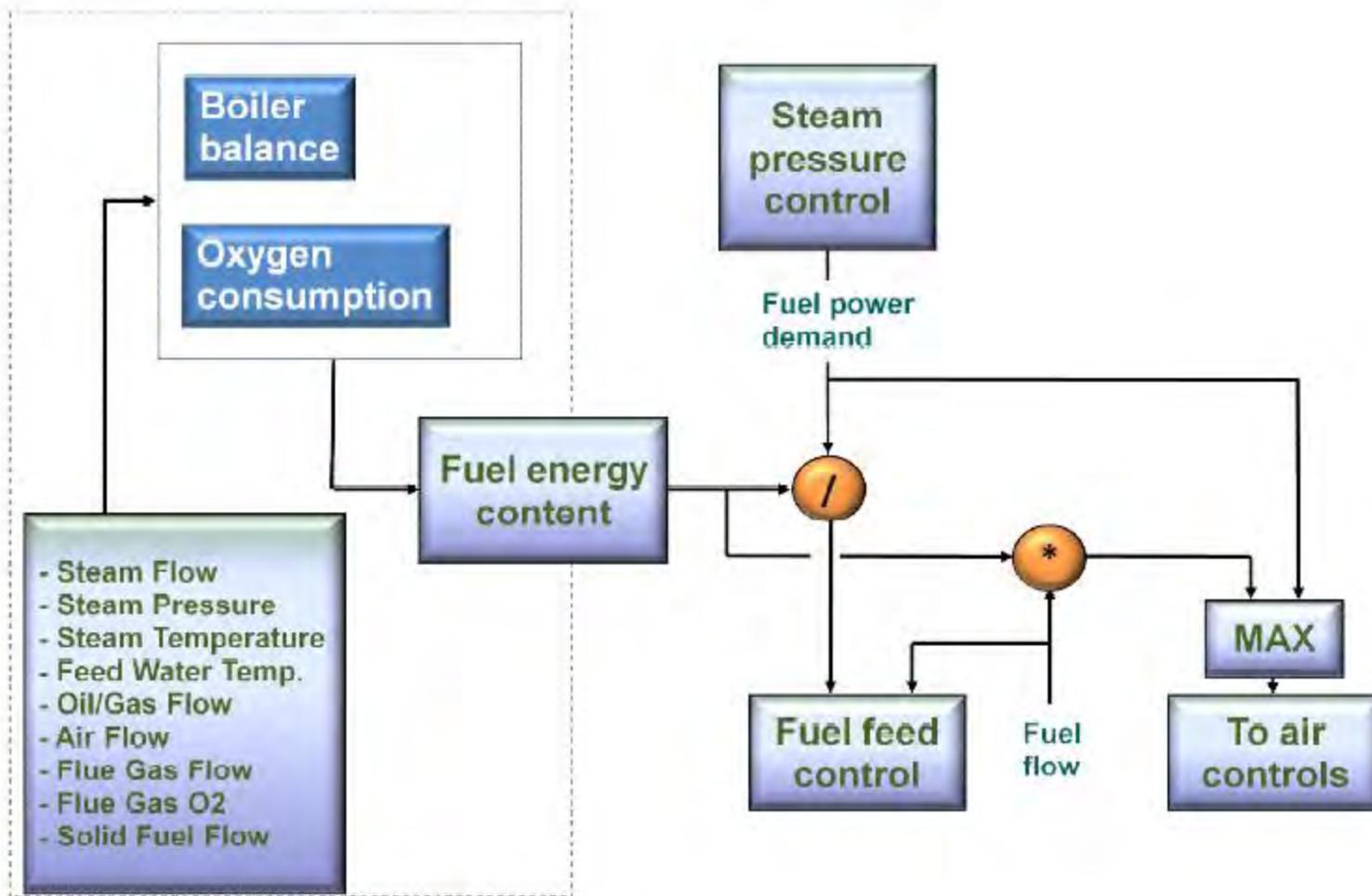


Boiler fuel control



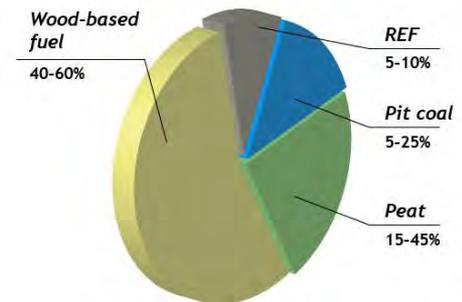
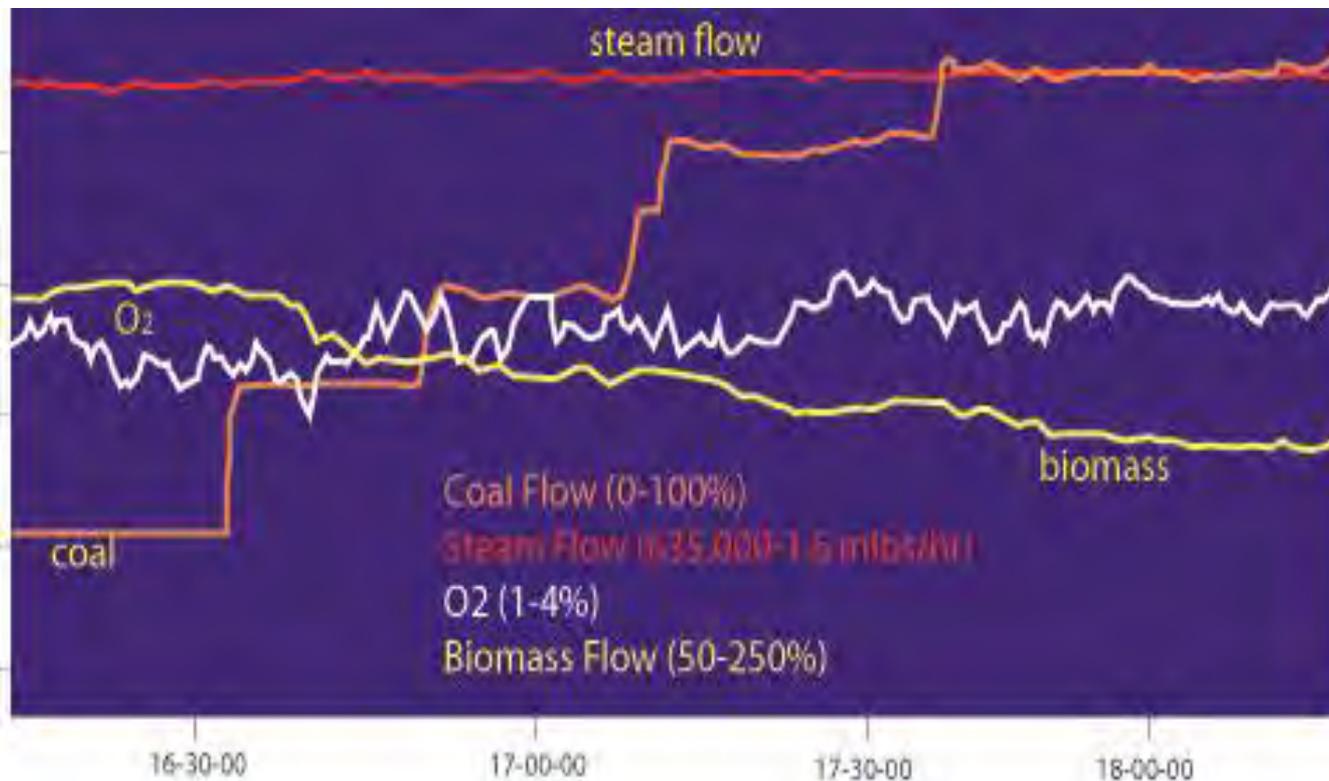
BTU Compensators should include the O₂ consumption

BTU Compensation input variables

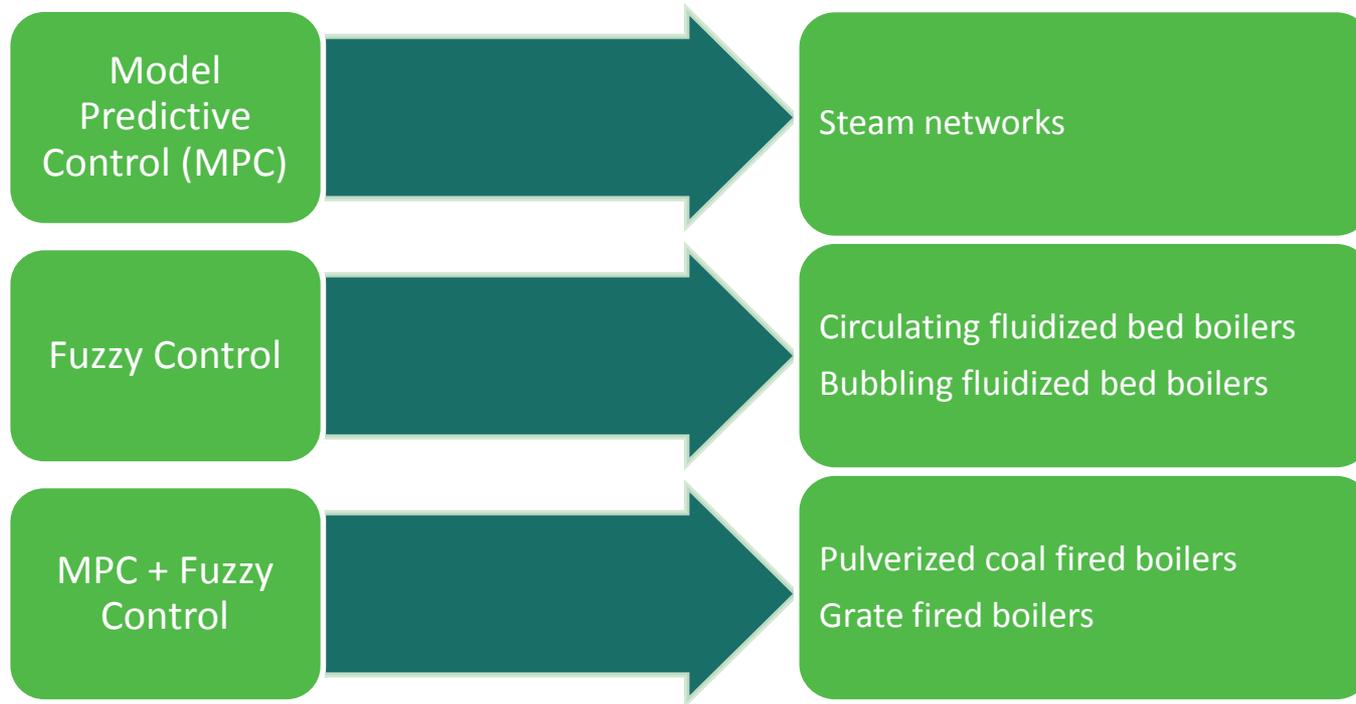


Performance at Alholmens 240MWe CFB plant

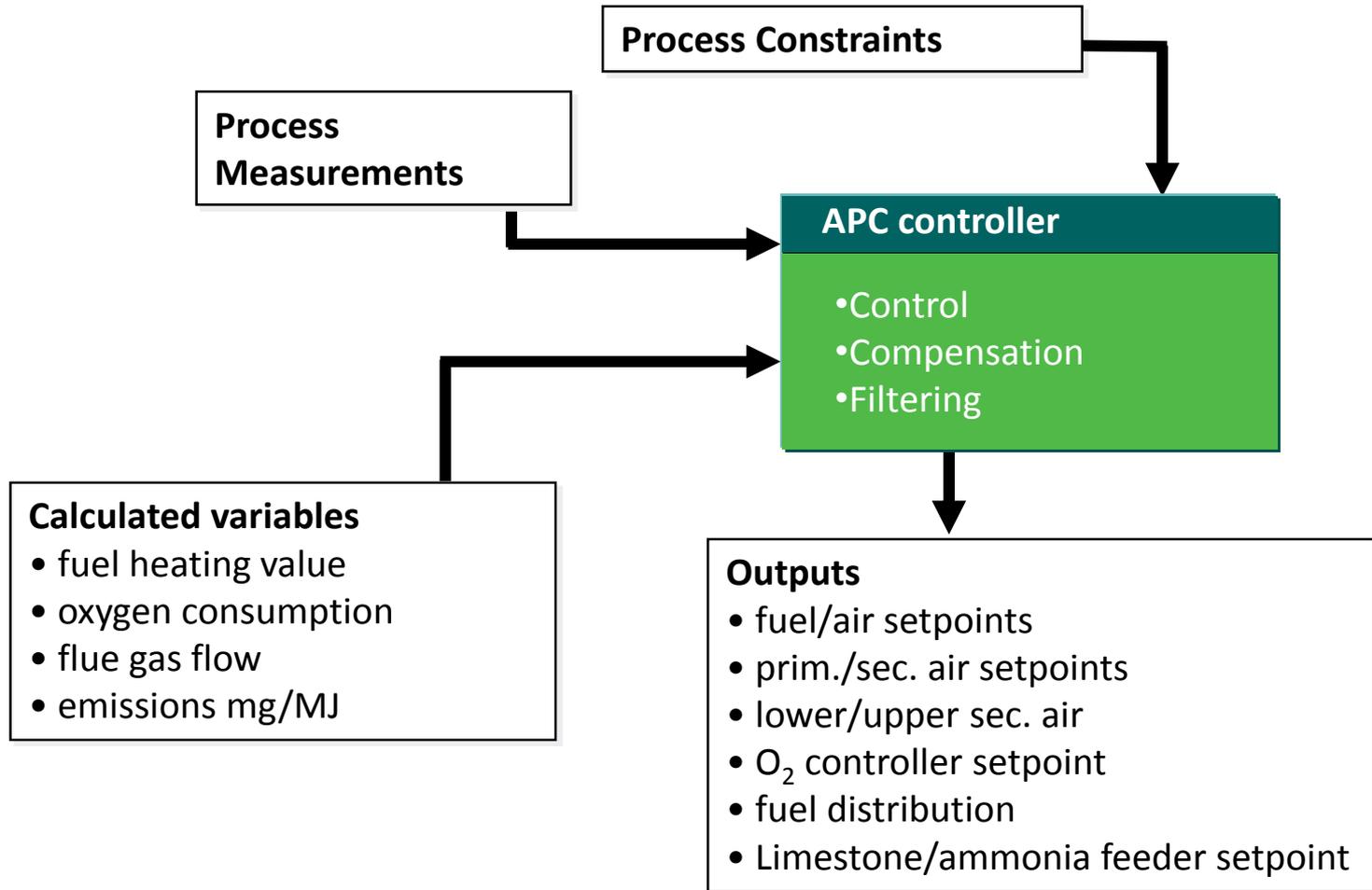
- Coal increased manually in 15% steps. Fuel control is automatically responding to increased heat release by driving the biomass downward to maintain constant energy out



Advance Process Control – The Technology



Combustion Manager – APC Structure



Multiple Input vs. PID controller

DNause D1U1/BOILER/Air Division optim.

Air Division optim. | IR_DIV_OPT

Control selection
RECIRC FLOW COEFF BIAS

Measurement selection	BED T ME-SP	BED TEMP GRA	STEAM LOAD	BED TEMP GRA	SF QF GRAD	NOT USED	NOT USED
Value	0.11	-0.09	805.05	-0.09	-0.12	0.00	0.00
Small	-20.00	-3.00	200.00	-5.00	-0.50	0.00	0.00
Normal_low	-5.00	-0.50	400.00	-0.50	-0.05	1.00	1.00
Normal_high	5.00	0.50	550.00	0.50	0.05	2.00	2.00
Big	20.00	3.00	600.00	5.00	0.50	3.00	3.00
Small	0.00	0.00	0.00	0.00	0.15	1.00	1.00
Normal	1.00	1.00	0.00	1.00	0.85	1.00	1.00
Big	0.00	0.00	1.00	0.00	0.00	1.00	1.00
Fault status	OK	OK	OK	OK	OK	OK	OK
Fault index	0	0	0	0	0	0	0

Function OK

Control OK

	1	2	3	4	5	6	7	8	9	10	11	12	13	14
ON/OFF	ON	ON	ON	ON	ON	OFF	OFF	OFF	OFF	ON	ON	ON	ON	ON
Control	Small	Small	Norm.	Big	Any	Any	Any	Any	Any	Any	Small	Norm.	Big	Big
Limit	Any	Any	Any	Any	Any	Any	Any	Any	Any	Any	Any	Any	Any	Any
Factor	0.00	0.00	0.00	0.00	0.15	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
Product	0.00	0.00	0.00	0.00	-0.46	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00

Sum of prod. -0.46

BLR-TIC-1005-20 F...

FLUIDIZED BED TEMP
CTL

0-2200 °F

M 1495.1

S 1500.0

L L 1500
R
C

0.0-0.8

0.37

F Auto

Grant Town Power Plant (West Virginia)

Problem: Each quarter I get dinged on operating costs, particularly limestone. Can I reduce limestone usage while still meeting my emissions requirements?



Facility facts

- Facility commissioned in 1992
- Boiler rated at 552 million Btu/hr
- Steam capacity 400,000 pounds per hour (Burns GOB fuel)
- Main steam conditions 955°F and 1370 psig
- Primary air injected above and under the grid. PA ~ 66% of total air
- Secondary air is injected into the dilute phase
- High pressure blowers to fluidize loop seal
- DCS: Foxboro IA series

The Goals...

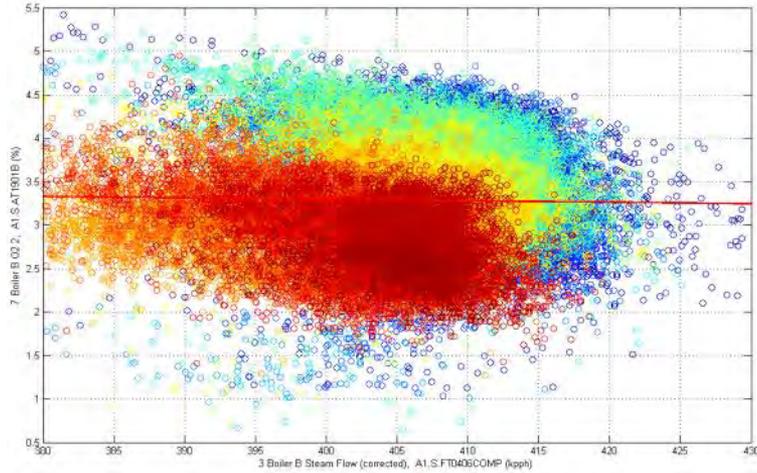
- Optimize combustion
- Reduce limestone consumption
- Maintain emission compliance

The Work...

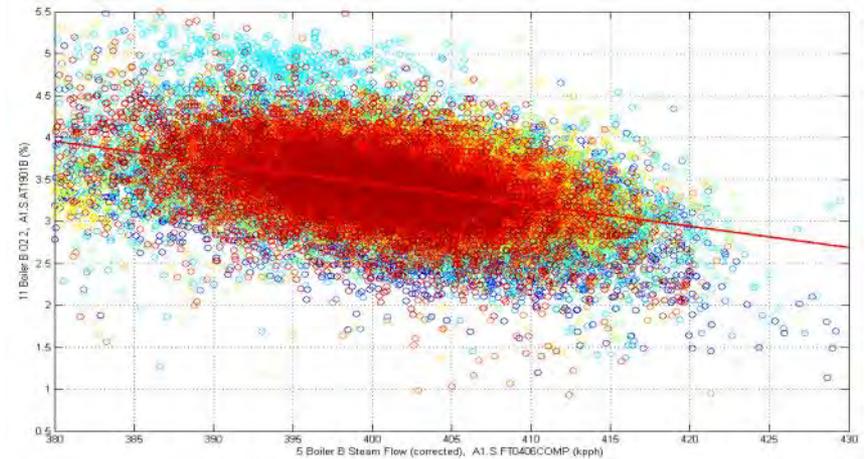
- Re-designed the air controls
- Modified fuel controls, bed level, and bed temp controls
- Valmet Advanced Process Controller added to control air distribution, fuel distribution, O₂ optimization and bed temperature optimization
- Valmet advanced BTU compensator to compensate for fuel quality fluctuations

Results: O2 vs. Steam Flow

2009

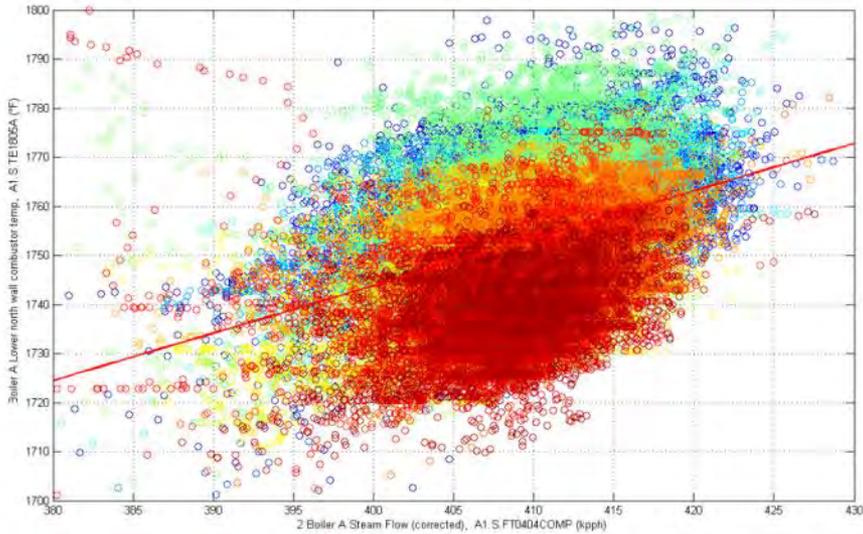


2011

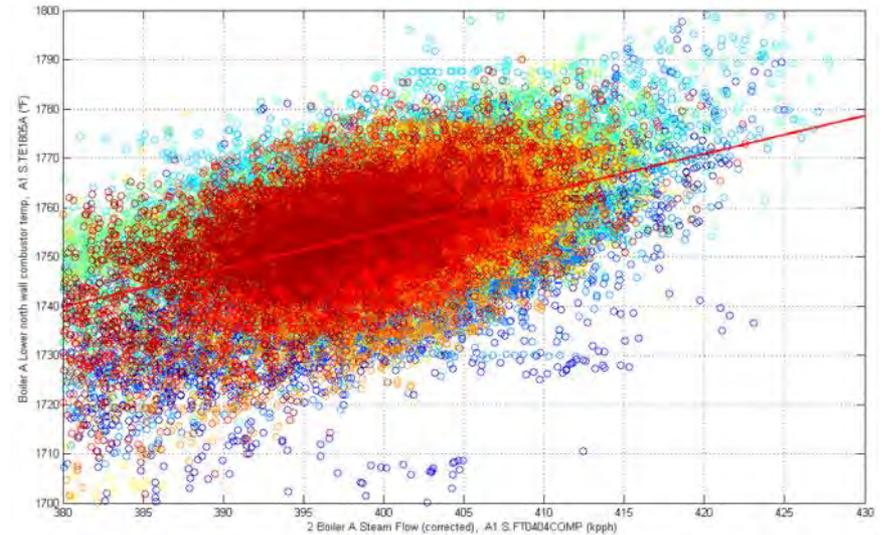


Results: Bed Temp Vs. Steam Flow

2009

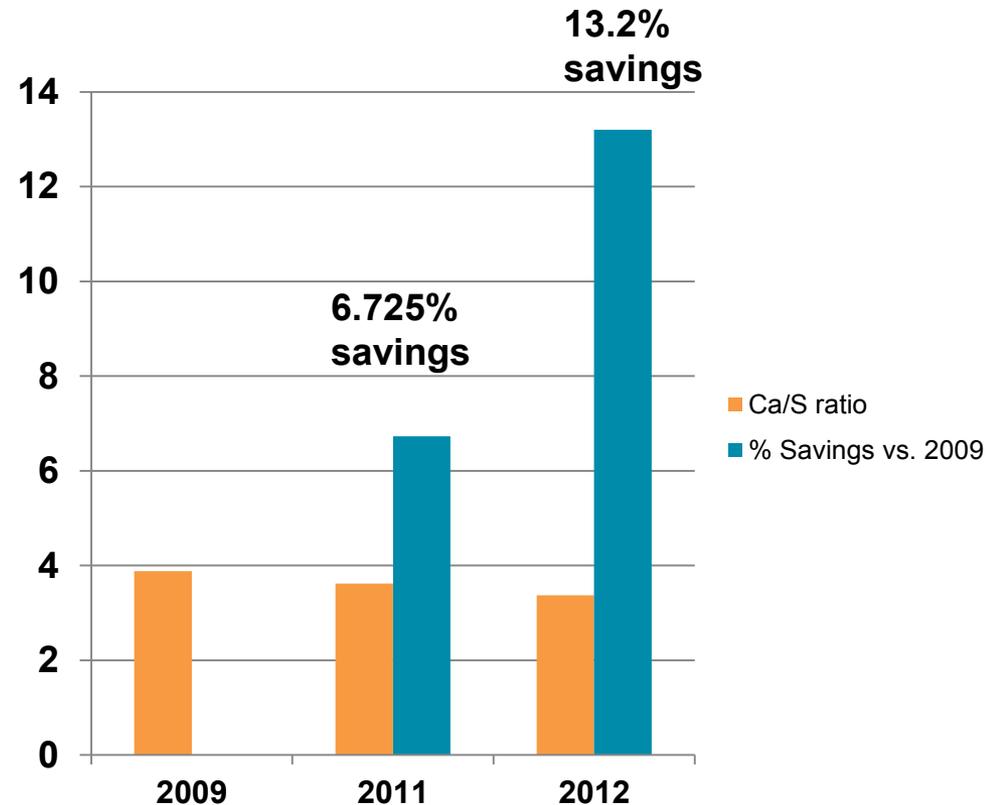


2011



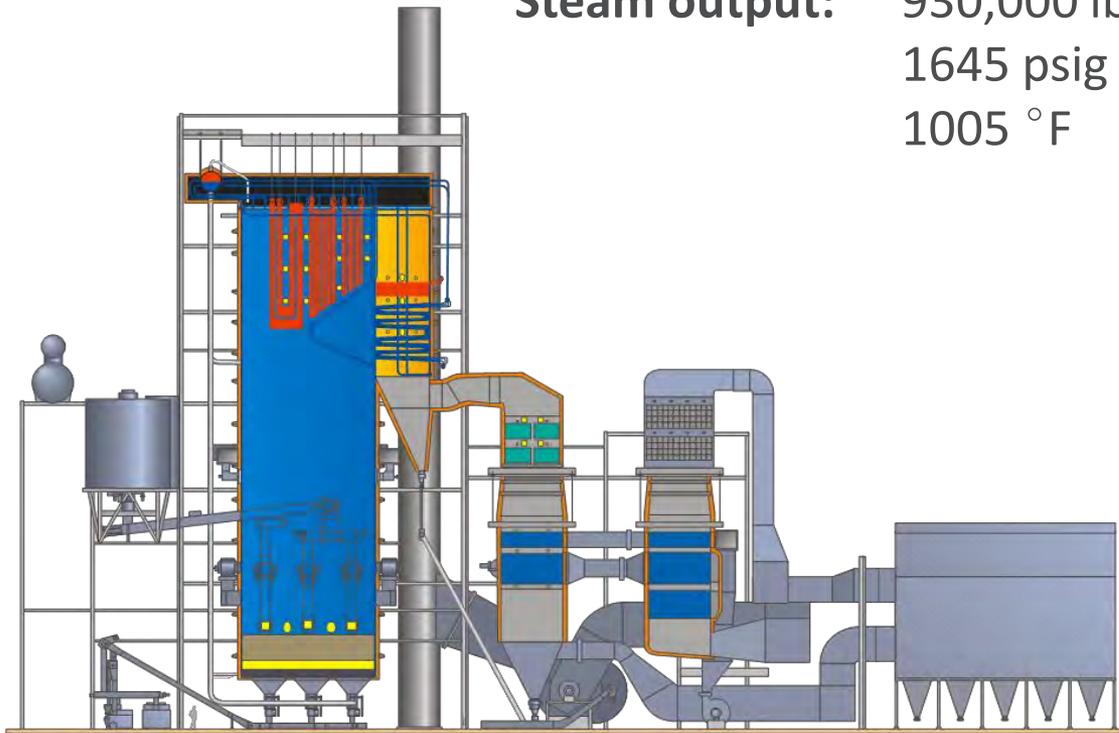
Sustainable results

- Operator acceptance excellent
- System in automatic greater than 90% of the time
- Operational uniformity across shifts



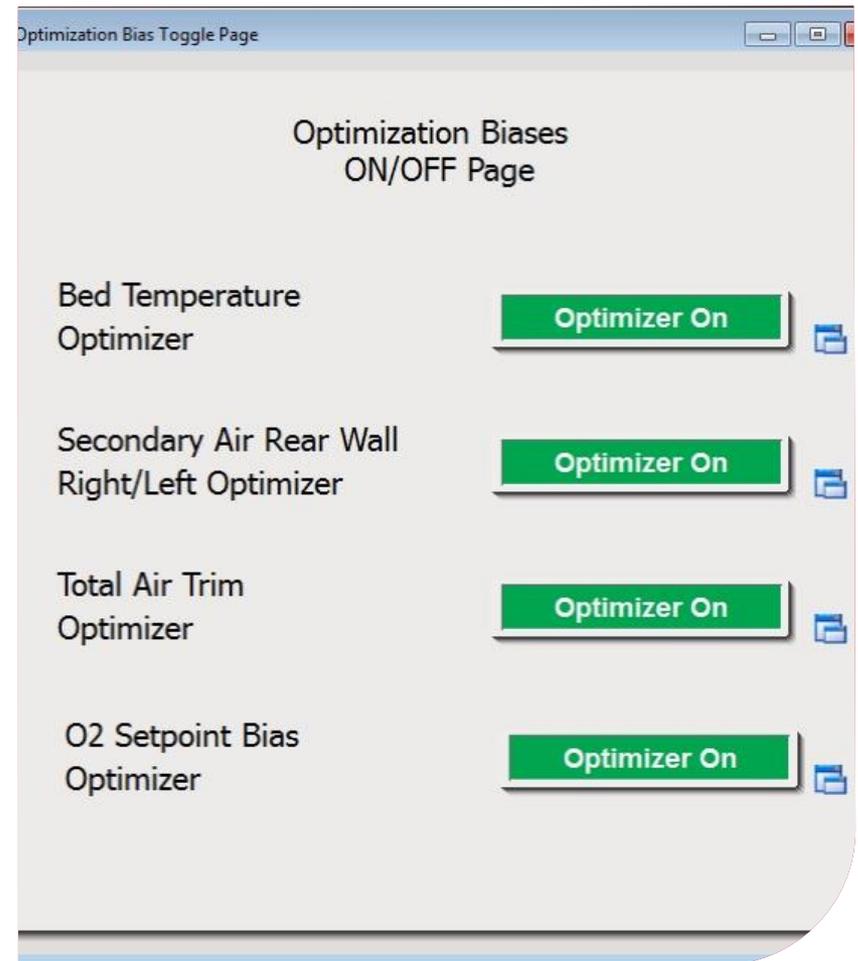
Valmet HYBEX boiler
Bubbling Fluidized Bed (BFB) technology

Steam output: 930,000 lbs/hr (100 MWe)
1645 psig
1005 °F



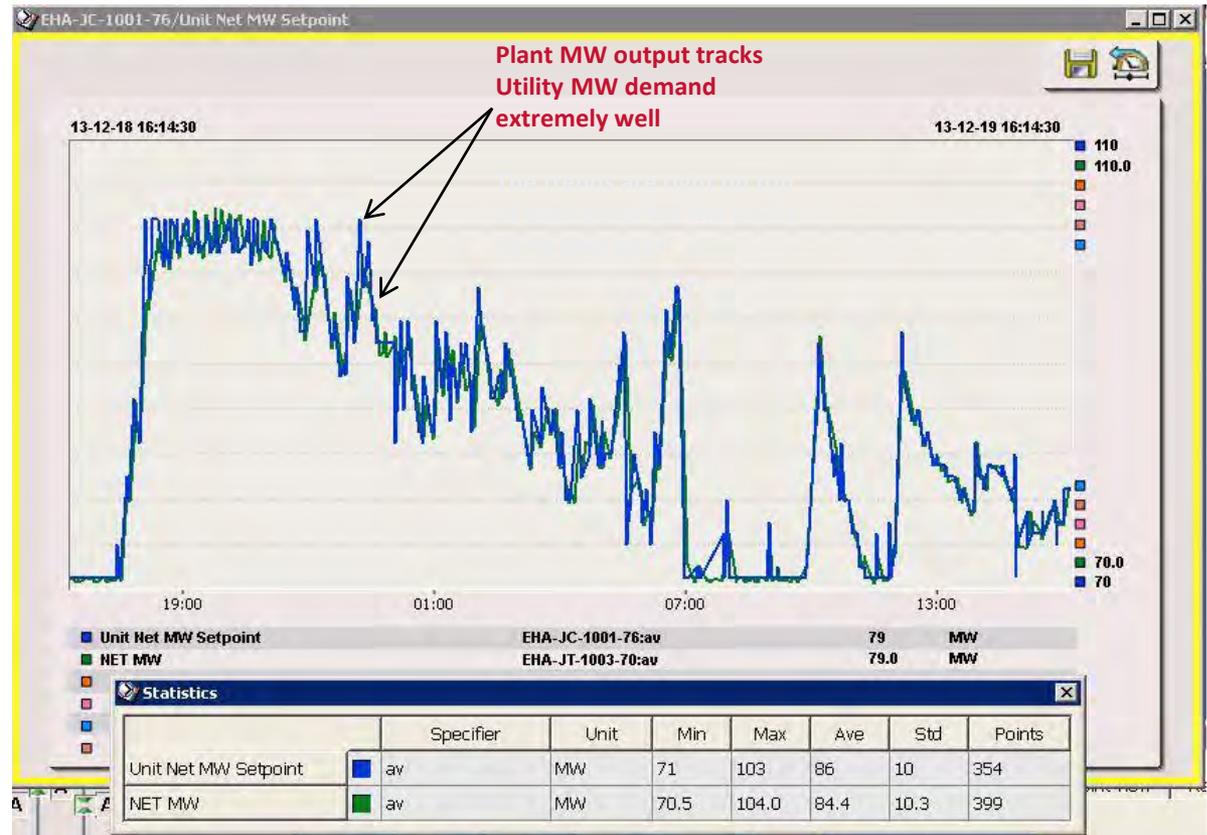
APC structure at GREC

- The system includes 4 advanced process controllers
- Bed temp APC minimizes bed temp & NO_x excursions especially during fast load changes
- Rear wall air distribution APC improves furnace symmetry
- Total air trim APC modifies total air demand based on fuel quality
- O2 trim APC optimizes between CO, NO_x and efficiency targets



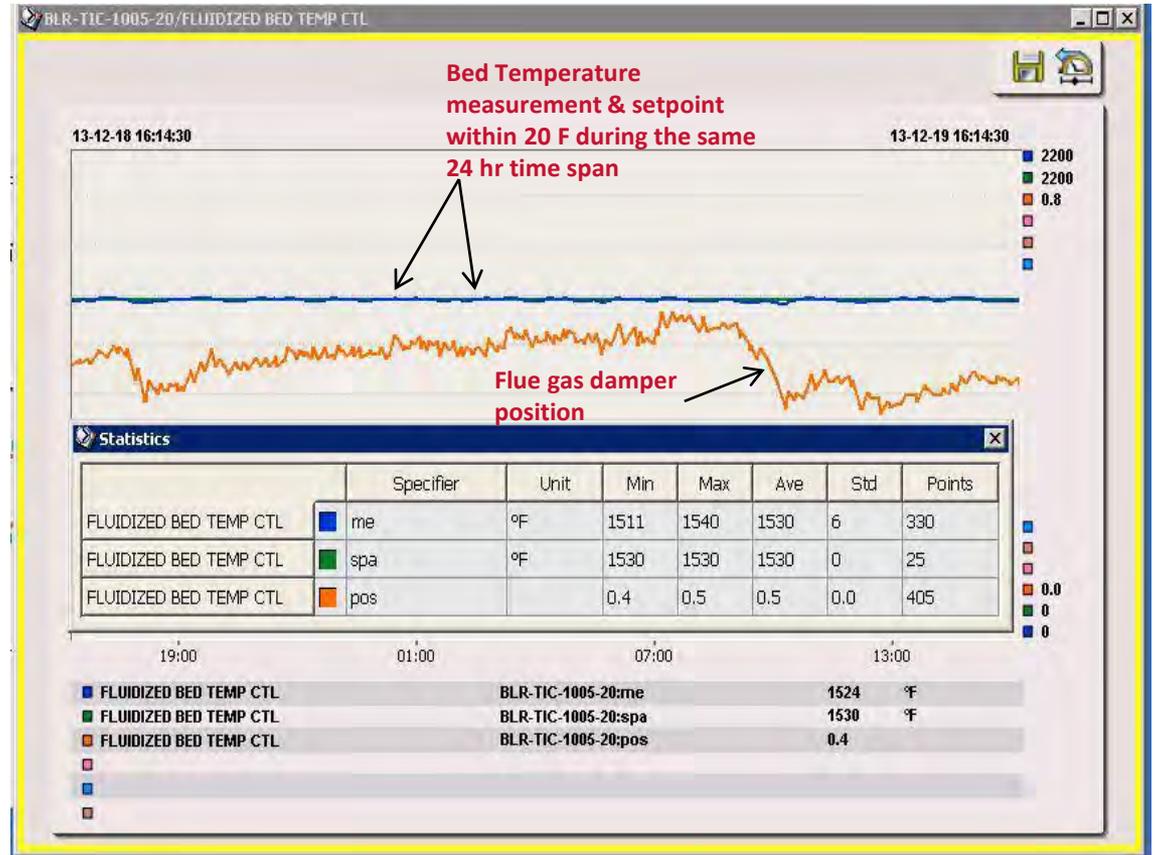
Unit load profile

- Unit load is dispatched at 3%/min
- Time span is 24 hrs
- Combustion controls run in automatic
- Metso's optimization controls have no trouble keeping up with load demand



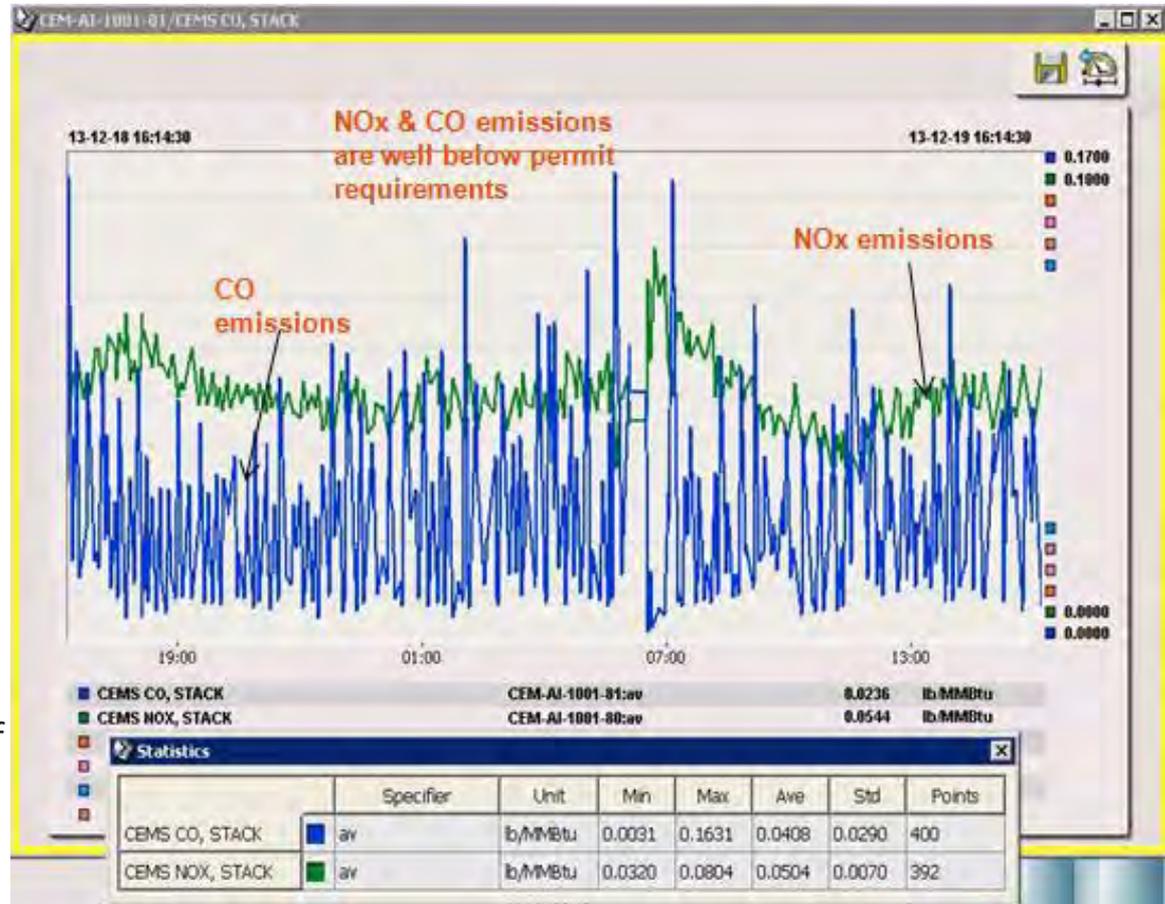
Bed temperature trend

- The bed temperature is very stable
 - Operator setpoint = 1530 F
 - Maximum measured value = 1540 F
 - Minimum measured value = 1511 F
- Standard deviation of 6 degrees F



CO & NO_x emissions

- The CO & NO_x emissions were below the permit requirements
- CO permit = 0.08 lbs/MMBTU
- Measured CO 24hr average = 0.0408 lbs/MMBTU
- NO_x permit = 0.07 lbs/MMBTU
- Measured NO_x 24hr average = 0.0504 lbs/MMBTU
- Measured average backpass O₂=2.3 %. The design setpoint of 2.8%
- Translates to a ~ 0.3% improvement in boiler efficiency



The take home message

- Process control with APC packages are going to be the new norm
- MPC & Fuzzy based controller technology are well established
- Projects typically pay for itself in less than a year but...
- Do your homework!
- No one size fits all solution
- And finally, optimization is a continuous process

